

PAC를 이용한 불소폐수 제거 효과

윤형선[†] · 박금주* · 양회남** · 이슬람*

한국산업단지공단 전남EIP사업단

*순천대학교 산업기계공학과

** (주)엔티스

Removal Effects of Fluorine Wastewater using PAC

Hyung-Sun Yoon · Keum-Joo Park* · Hwoi-Nam Yang** · Mohammad N. Islam*

Jeonnam Eco-Industrial Park Development Division, Korea Industrial Complex Corp.

**Department of Industrial Machinery Engineering, Suncheon National University*

***ENTIS Co., Ltd.*

ABSTRACT

This paper describes the pH and PAC effect on the reduction of fluorine contained in industrial wastewater. We tried to find out the actual pH value and PAC which can make the best treatment efficiency. The main chemistry of this process is precipitation-coagulation. In this experiment, we used a small amount of $\text{Ca}(\text{OH})_2$ for generating CaF_2 and two types of PAC for making $\text{Al}(\text{OH})_3$ flock to adsorb fluorine and an aluminate ion. The best removal efficiency was obtained at pH 10, and PAC 2 (12% of AlO_3) can produce good treating condition than PAC 1 (17% of AlO_3) for low concentration and high concentration fluorine wastewater, respectively. We expect this method will make a significant contribution to treat the fluorine contained industrial waste water with short reaction time and easy handling.

Keywords : Poly aluminum chloride (PAC), Wastewater treatment, Fluorine, pH, Removal efficiency

[†]Corresponding author E-mail: yhsecl@hanmail.net

1. Introduction

Fluoride is often present in a variety of untreated industrial effluents, including those from chemical plants manufacturing organic fluorine compounds, aluminum smelters, phosphate fertilizers, semiconductor manufacturing, glass and brick making industries, and coal power plants^{3),13),15)}. The concentrations of fluoride in untreated industrial waste waters vary widely, and concentrations as high as 500 to 2,000 mg/L have been reported in effluents from semiconductor industry operations^{5),6)}. Various treatment technologies based on precipitation¹⁰⁾, ion exchange⁹⁾, adsorption^{17),18)}, membrane process such as reverse osmosis²⁾, nanofiltration⁷⁾, electrodialysis^{1),14)}, and electro-chemical technology, including electro-coagulation, electro-flotation and electro-chemical oxidation⁸⁾, have been proposed for removal of fluoride from wastewater.

The industrial working process, which requires extremely high precision, generates both environmental and hazardous wastes.¹⁶⁾ Some of previous studies prove that fluorine in water and wastewater can be treated to a desirable limit by adsorption or precipitation⁴⁾. Calcium salt and aluminum salt or lime precipitation of fluoride can reduce the residual fluoride concentration to 10–15 mg/L or lower^{11),12)}.

The most cost effective and common treatment method to remove fluorine is

calcium salt precipitation. This method has also operational convenience and short reaction time. The salt is implemented by adding fixed amount of calcium salt which reacts with fluorine ions in the wastewater.



It is two steps treatment process i.e. CaF_2 formation and fluorine adsorption by $\text{Al}(\text{OH})_3$. First produces CaF_2 sludge and secondly generates a large amount of fluorine containing $\text{Al}(\text{OH})_3$ sludge.

Removing fluorine from wastewater : Generally fluorine contained wastewater treatment system is described into five processes. Each process is described as follows.

1) With pH control, the wastewater containing fluorine produces a calcium fluoride (CaF_2) by adding calcium salt and in this process a small amount of sludge is produced also.

2) Sludge is separated from first treated water by solid-liquid separation.

3) Again, with pH control, the first effluent generates aluminum fluoride or makes $\text{Al}(\text{OH})_3$ flock by adding aluminum compounds. The theoretical quantity of adding calcium is ; Calcium : fluorine = 1 : 2

4) The waste sludge is separated by solid-liquid separation.

5) Finally, the waste sludge is gone into the dehydrator.

Our current research also involves these

concepts. The objective of this study is to evaluate the pH and PAC effects on the reduction of fluorine concentration from the industrial wastewater.

2. Materials and Method

2.1. Experimental

Fluorine wastewater of low concentration (142 mg/L) and high concentration (1520 mg/L) was collected from Yeosu Industrial Complex area, South Korea. Initial pH was 3.7 and 3.01, respectively. This experiment was done two times for confirm in g the actual treating condition. Experiment was carried o ut using lab scale Jar reactor with controlling mixing speed(200 rpm) at farm power lab in Sunchon National University, South Korea. We tried to find out the pH(7, 8, 9, and 10) effects for the low concentration waste water and the PAC

effects for high concentration fluorine waste water at the pH 7. Both experiments were done with same procedure. In the first step, CaF_2 (sludge 1) is generated, and fluorine adsorbing $\text{Al}(\text{OH})_3$ (sludge 2) is generated in the second step. The quantity of sludge 2 is much larger than that of sludge 1. Therefore, the main part of total sludge generated is the $\text{Al}(\text{OH})_3$ sludge produced in the second step.

2.2. Materials

The fluorine wastewater was used as a feed after diluting a concentrated calcium hydroxide for increasing pH. After 1st effluent, we used aluminum salt such as PAC in the second treatment. This experiment was done by using lab scale jar reactor.

2.3. Analytical

After settling the $\text{Al}(\text{OH})_3$ flock at the bottom of reactor, we took the samples from the supernatant for measuring the fluorine

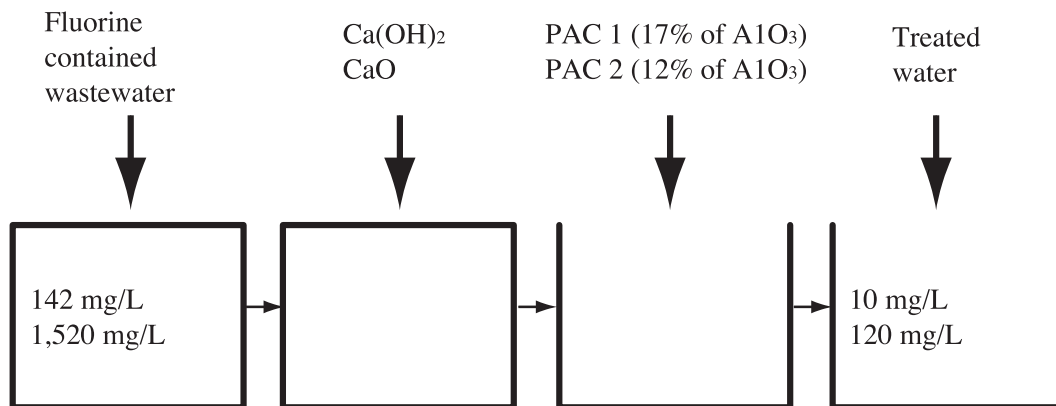


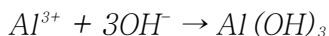
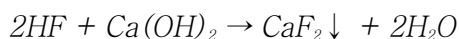
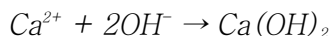
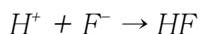
Fig. 1. Process flow diagram.

concentration. It was measured according to standard methods published by the American Public Health Association (APHA, 1998), using a DR/2800 spectrophotometer (Hatch, 1993).

2.4. Principle of treatment process

The main chemistry of this process is the conventional precipitation. The ion

product (Ca^{2+} and F^-) by applying calcium hydroxide is formed into CaF_2 in the homogeneous liquid phase according to the following reaction.



Finally, fluorine adsorbing $\text{Al}(\text{OH})_3$ sludge is separated from the water and settles at the bottom of it.

3. Result and Discussion

3.1. Effect of pH

For this experiment we collected actual wastewater from Yeosu industrial complex area. For treating low concentration of fluorine wastewater, $\text{Ca}(\text{OH})_2$ was used to form CaF_2 , and PAC 2 (12% of AlO_3) was added to make $\text{Al}(\text{OH})_3$ flock with different pH (7, 8, 9 and 10).

Fig. 2 shows the relationship between the

pH and the concentration of fluorine in treated water. As shown in the figure, fluorine in wastewater was removed down to a low concentration. Comparing among pH, we got the lower value of fluorine 10.2 mg/L with 92.81% fluorine removal efficiency at pH 10 (Table 1).

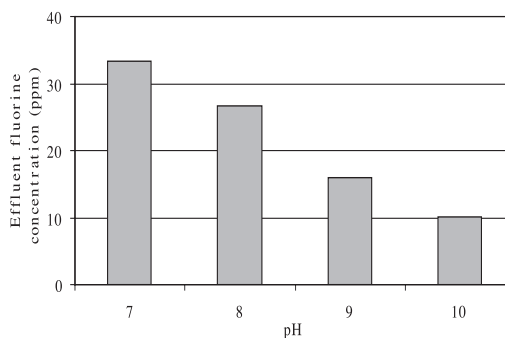


Fig. 2. Relationship between pH and fluorine concentration in effluent water.

3.2. Treatment performance of PAC

For high concentration fluorine wastewater (1520 mg/L), we used CaO for the first treatment and PAC 1 (17% of AlO_3) and PAC 2 (12% of AlO_3) for the second treatment with controlling pH 7. In the second treatment PAC 1 of 350 ppm has the same value of AlO_3 with PAC 2 (12%) of 496 ppm. We found out the PAC effect to treat this wastewater. Table 2 shows that better effluent was obtained from the PAC 2 of 496 ppm than from the PAC 1 of 350 ppm. Using PAC 1, we got the final fluorine concentration 240 mg/L with 92.1% of removal efficiency and using PAC 2, we got 120 mg/L with 84.21% of removal efficiency

Table 1. Treatment procedure of low concentration fluorine wastewater

No	1st Treatment ; 25% Ca(OH) ₂ 20 min reaction + 20 min settle			2nd Treatment ; PAC 2(12% of AlO ₃) 20 min reaction + 20 min settle			
	Quantity (Raw water) (ml)	pH	Input Ca(OH) ₂ (ml)	1st effluent (ml)	Input (PAC 2) (ppm)	Final Conc. (mg/L)	Removal efficiency (%)
1	600	7	0.7	500	80	33.4	76.47
2	600	8	0.8	500	80	26.6	81.26
3	600	9	0.9	500	80	16.0	88.73
4	600	10	1.1	500	80	10.2	92.81
Influent wastewater fluorine concentration=142 mg/L							

Table 2. Treatment procedure of high concentration fluorine wastewater

Reagent	Treatment			2nd Treatment			Removal efficiency (%)
	Quantity (Raw water) (ml)	pH	Input CaO, (gm)	1st effluent (ml)	Input PAC (ppm)	Final Conc. (mg/L)	
PAC 1	600	7	9.61	500	350	240	84.21
PAC 2	600	7	9.61	500	496	120	92.10
Influent wastewater fluorine concentration=1520 mg/L							

4. Conclusion

This study demonstrates that industrial wastewater containing fluorine can be efficiently treated by precipitation method. The combined use of calcium salt and PAC can be a process to enhance the removal efficiency. Comparing PAC1 (17% of AlO₃) and PAC 2 (12% of AlO₃), we obtained the better efficiency from PAC2. It is very important to select the pH value and PAC

which influence on the fluorine removal efficiency.

Acknowledgement

This research was supported by the program for the construction of Jeonnam Eco-Industrial Park(EIP) which was conducted by the Korea Industrial Complex Corporation (KICOX) and the Ministry of Knowledge Economy (MKE).

References

1. Amor, Z., Bariou, B., Mameri, N., Taky, M., Nicolas, S. and Elmidaoui, A.(2001). Fluoride removal from Corn brackish water by electrodialysis. *Desalination*. 133. pp.215~223.
2. Bouguecha, S. and Dhahbi, M.(2002). The role of membrane technologies in supplying drinking and industrial water in Tunisia: conventional process and new trends. *Desalination*. 151. pp.75~86.
3. Camargo, J.A.(2003). Fluoride toxicity to aquatic organisms:A review. *Chemosphere*. 50. pp.251~264.
4. Hao, O.J. and Huang, C.P.(1986). Adsorption characteristics of fluoride into hydrous alumina. *Journal of Environmental Enh. Div. ASCE*. 112. pp.1054~1069.
5. Hu, C.Y., Lo, S.L., Kuan, W.H. and Lee, Y.D.(2005). Removal of fluoride from semiconductor wastewater by electrocoagulation-flotation. *Water Res.* 39. pp.895~901.
6. Huang, C.J. and Liu, J.C.(1999). Precipitate flotation of fluoride containing waste-water from a semiconductor manufacturer. *Water Res.* 33. pp.3403~3412.
7. Hu,K. and Dickson, J.M.(2006). Nanofiltration membrane performance on fluoride removal from water. *J. Membr. Sci.* 279. pp.528~529.
8. Jiantuan, J., Jiuhui, Q., Pengju, L. and Huijuan, L.(2004). New bipolar electro-coagulation lectro-flotation process for the treatment of laundry wastewater. *Sep. Purif. Technol.* 36. pp.33~39.
9. Kodama, H. and Kabay, N.(2001). Reactivity of inorganic anion exchanger BiPbO₂(NO₃) with fluoride ions in solution. *Solid State Ionics*. 141. pp.603~607.
10. Mameri, N., Yeddou, A.R., Lounici, H., Belhocine, D., Grib, H. and Bariou, B.(1998). Defluorination of septentrional Sahara water of North Africa by electro coagulation process using bipolar aluminum electrodes. *Water Res.* 32. pp.1604~1612.
11. Parthasarathy N., Buffle J. and Haerdi, W.(1986). Combined use of calcium salts and polymeric aluminum hydroxide for defluorid- ation of wastewaters. *Water Res.* 20. pp.443 ~448.
12. Saha, S.(1993). Treatment of aqueous effluent for fluoride removal. *Water Res.* 27. pp.1347~1350.
13. Shen, F., Chen, X.M., Gao, P. and Chen, G.H.(2003). Electrochemical removal of fluoride ions from industrial wastewater. *Chem. Eng. Sci.* 58. pp.987~993.
14. Tahaikt, M., Achary, I., Menkouchi Sahli, M.A., Amor, Z., Taky, M., Alami, A., Boughriba, A., Hafsi, M. and Elmidaoui, A.(2004). Defluoridation of Moroccan ground water by electrodialysis: continuous operation. *Desalination*. 167. pp. 357~365.

15. Valeria, O-H., Qais, B., Glendy, L., Chandra, K., James, A.F. and Reyes, S-A.(2009). Toxicity of fluoride to microorganisms in biological wastewater treatment systems. *Water Res.* 43. pp.3177~3186.
16. Vagliasindi, F. G. and Poulson, S. R.(1994). Waste generation and management in the semiconductor industry: a case study. *Water Sci. Tech.* 29. pp.331~341.
17. Yang,C.L. and Dluhy,R.(2002). Electrochemical generation of aluminum sorbent for fluoride adsorption, *J. Hazard. Mater. B.* 94. pp.239~ 252.
18. Zhou, Y., Yu, C. and Shan, Y.(2004). Adsorption of fluoride from aqueous solution on La^{3+} impregnated cross linked gelatin, *Sep. Purif. Technol.* 36. pp.89~94.

